Please amend the Application as follows.

IN THE CLAIMS:

This listing of claims will replace all prior versions, and listings of claims in the application.

1 (Original). A process for the purification of toluene diisocyanate from a crude distillation feed comprising less than 2% by weight of phosgene comprising

a) fractionating the crude distillation feed comprising less than 2% by weight of phosgene to remove solvent and, optionally, reaction residue to produce a crude toluene diisocyanate feed comprising less than 20% by weight of solvent and

b) separating the crude toluene diisocyanate feed comprising less than 20% by weight of solvent in a divided-wall distillation column into four product fractions P1 – P4 comprising:

P1, a vapor phase low-boiler and solvent-enriched gas stream,

P2, a low-boiler and solvent–enriched product,

P3, a high-boiler-enriched bottoms product comprising toluene diisocyanate and

P4, a toluene diisocyanate product stream lean in low-boiler, high-boiler and reaction residue.

2 (Currently amended). The process of Claim 1 in which the product fraction P1 comprises 20-99% by weight of the solvent, the low-boiler and toluene diisocyanate.

3 (Currently amended). The process of Claim 1 in which the product fraction P2 comprises the solvent, the low boiler and toluene diisocyanate.

4 (Currently amended). The process of Claim 1 in which the product fraction P3 comprises toluene diisocyanate and 0.5-15% by weight of ~~a~~ the high boiler.

5 (Currently amended). The process of Claim 1 in which the product fraction P4 has a toluene concentration of at least 99.5% by weight and comprises less than 200 ppm by weight of the solvent and/or chlorinated aromatic hydrocarbon, less than 100 ppm by weight hydrolyzable chlorine and less than 40 ppm by weight acidity.

6 (Currently amended). A process for the production of toluene diisocyanate comprising:

a) reacting toluene diamine with phosgene to produce a crude distillation feed,

b) separating any unreacted phosgene present in an amount greater than or equal to 2% by weight from the crude distillation feed if the crude distillation feed comprises 2 % by weight or more of phosgene to obtain a crude distillation feed comprising less than 2% by weight of phosgene,

c) fractionating the crude distillation feed comprising less than 2% by weight of phosgene to remove the solvent and optionally the reaction residue to produce a crude toluene diisocyanate feed comprising less than 20% by weight of the solvent and

d) separating the crude toluene diisocyanate feed comprising less than 20% by weight of the solvent in a divided-wall distillation column into four product fractions P1 – P4 comprising:
P1, a vapor phase low-boiler and solvent-enriched gas stream,
P2, a low-boiler and solvent–enriched product,
P3, a high boiler enriched bottoms product comprising toluene diisocyanate and
P4, a toluene diisocyanate product stream lean in low-boiler, high-boiler and reaction residue.

7 (Currently amended). The process of Claim 6 in which the product fraction P1 comprises 20 – 99% by weight of the solvent, the low-boiler and toluene diisocyanate.

8 (Currently amended). The process of Claim 6 in which the product fraction P2 comprises the solvent, the low boiler and toluene diisocyanate.

9 (Currently amended). The process of Claim 6 in which the product fraction P3 comprises toluene diisocyanate and 0.5-15% by weight of the high-boiler.

10 (Currently amended). The process of Claim 6 in which the product fraction P4 has a toluene diisocyanate concentration of at least 99.5% by weight and comprises less than 200 ppm by weight of the solvent and / or chlorinated aromatic hydrocarbons, less than 100 ppm by weight hydrolyzable chlorine and less than 40 ppm by weight acid~~ity~~.